

# PHY524 Cryogenics-3

Cryocoolers

11/13/2025

Material adopted from

1. <https://www.stonybrook.edu/commcms/case/courses/PHY695>
2. <http://cryocourse2016.aalto.fi/#program>
3. <http://cryocourse2011.grenoble.cnrs.fr/spip.php%3Frubrique13.html>
4. [USPAS | Materials | by Year | 21onlineSBU | Cryogenic Engineering](#)
5. [USPAS | Materials | by Year | 10MIT | Cryo Engineering](#)

# Cryo-coolers

Different types:

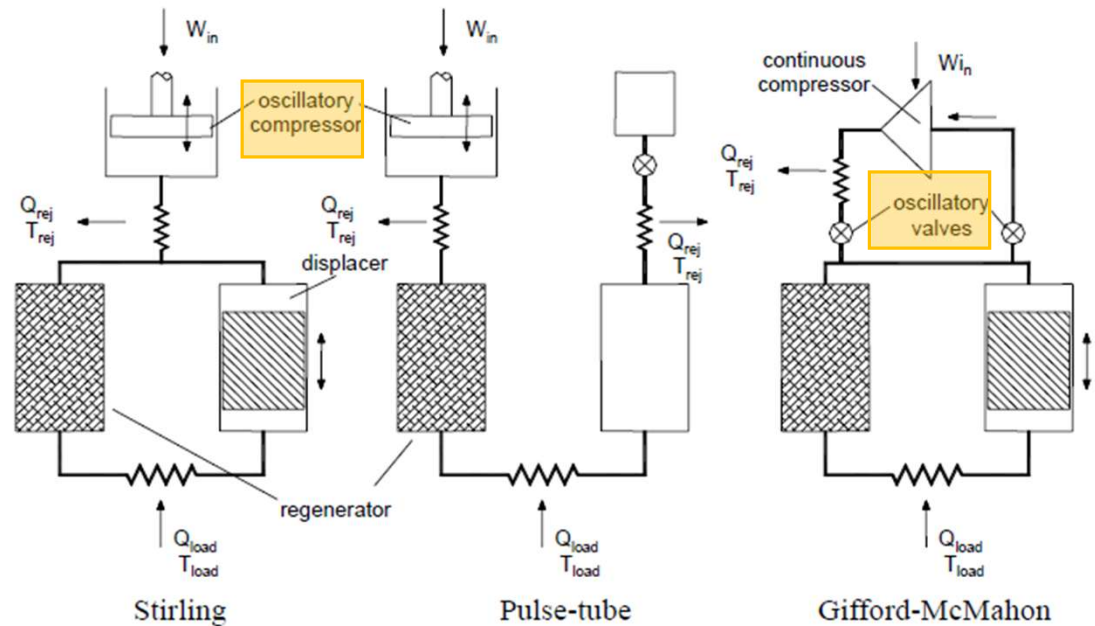
## Oscillating gas flow cryocoolers

- Stirling refrigerators
- Gifford-McMahon (GM) refrigerators
- Pulse-tube refrigerators

## Constant gas flow cryocoolers (next lecture)

- Joule-Thomson cooler
- Dilution refrigerators

## Regenerative Systems



Oscillatory flow: frequencies 1 - 100 hz

Regenerative heat exchangers: ideal – zero void volume,  $\Delta P$ , high  $c_p$

Phase modulation (between pressure and flow waves) is crucial for performance

# Stirling cycle and Stirling engines

## Stirling cycle engine:

- invented in 1815
- 1950's bid for auto industry
- Today: 2.5 kW generators

- Stirling cryocoolers: 1946 -

- Ideal efficiency = Carnot

- $COP = T_c / (T_h - T_c)$

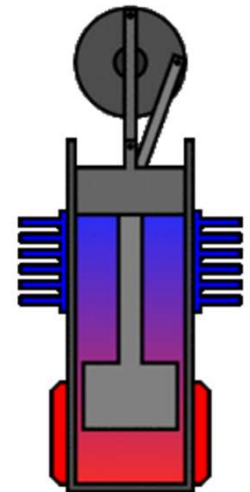
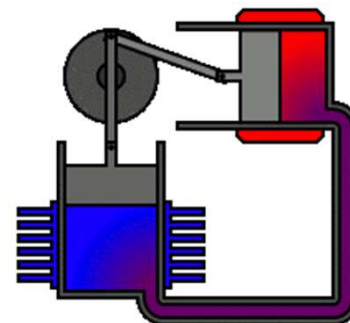
- Primary uses:

- tactical and security IR systems
- medical and remote- location cryogen plants

- Potential cooling for large scale HTS applications

- Commercial sources:

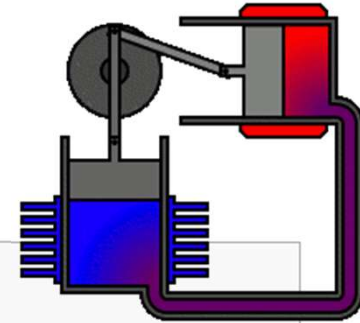
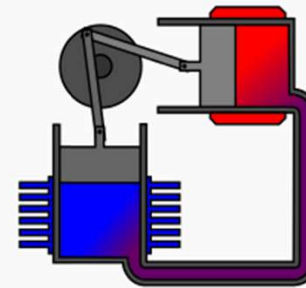
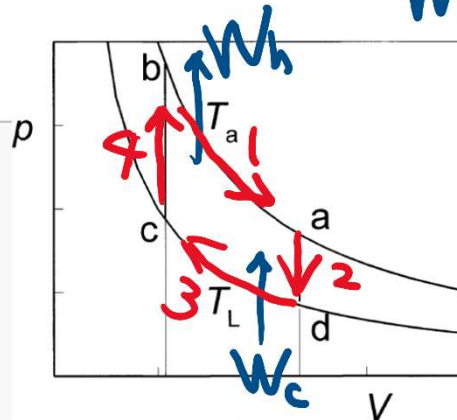
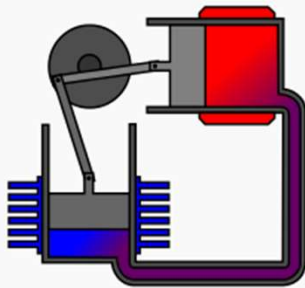
- Stirling ([www.stirling.nl](http://www.stirling.nl))
- Sunpower ([www.sunpower.com](http://www.sunpower.com))
- Stirling Technology Company([www.stirlingtech.com](http://www.stirlingtech.com))



# Stirling alpha engine

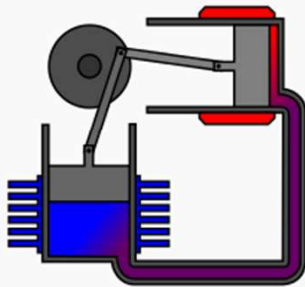
[https://en.wikipedia.org/wiki/Stirling\\_engine](https://en.wikipedia.org/wiki/Stirling_engine)

$$W = \int F \cdot ds = P \cdot \Delta V$$

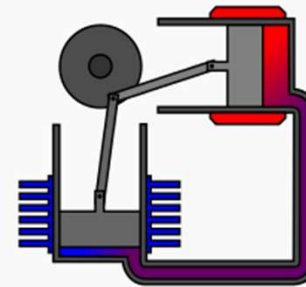


1. Most of the working gas is in the hot cylinder and has more contact with the hot cylinder's walls. This results in overall heating of the gas. Its pressure increases and the gas expands. Because the hot cylinder is at its maximum volume and the cold cylinder is at the top of its stroke (minimum volume), the volume of the system is increased by expansion into the cold cylinder.

2. The system is at its maximum volume and the gas has more contact with the cold cylinder. This cools the gas, lowering its pressure. Because of flywheel momentum or other piston pairs on the same shaft, the hot cylinder begins an upstroke reducing the volume of the system.



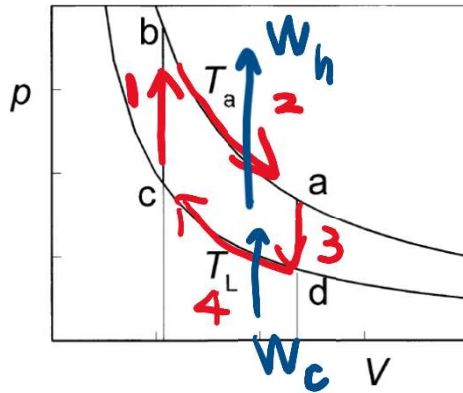
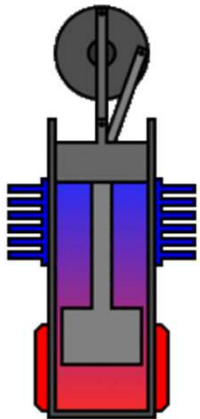
CW: heat  $\rightarrow$  work



3. Almost all the gas is now in the cold cylinder and cooling continues. This continues to reduce the pressure of the gas and cause contraction. Because the hot cylinder is at minimum volume and the cold cylinder is at its maximum volume, the volume of the system is further reduced by compression of the cold cylinder inwards.

4. The system is at its minimum volume and the gas has greater contact with the hot cylinder. The volume of the system increases by expansion of the hot cylinder.

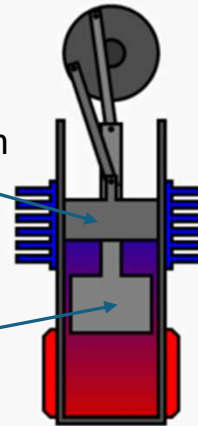
# Stirling beta engine



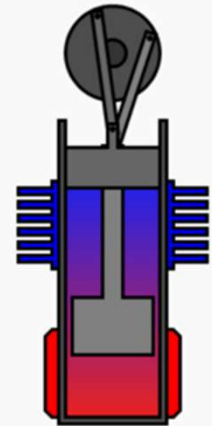
[https://en.wikipedia.org/wiki/Stirling\\_engine](https://en.wikipedia.org/wiki/Stirling_engine)

Power piston

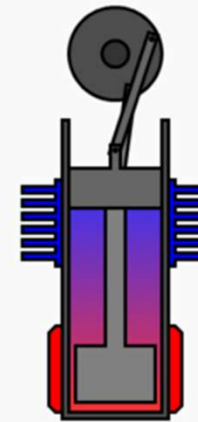
Displacer piston



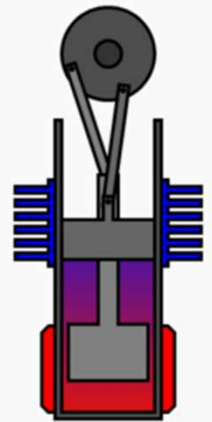
1. Power piston (dark grey) has compressed the gas, the displacer piston (light grey) has moved so that most of the gas is adjacent to the hot heat exchanger.



2. The heated gas increases in pressure and pushes the power piston to the farthest limit of the **power stroke**.



3. The displacer piston now moves, shunting the gas to the cold end of the cylinder.



4. The cooled gas is now compressed by the flywheel momentum. This takes less energy, since its pressure drops when it is cooled.



# Stirling Coolers

The thermal contact with the surroundings at the temperatures  $T_a$  and  $T_L$  is supposed to be perfect so that the compression and expansion are **isothermal**.  
Constant volume: **isochoric**.

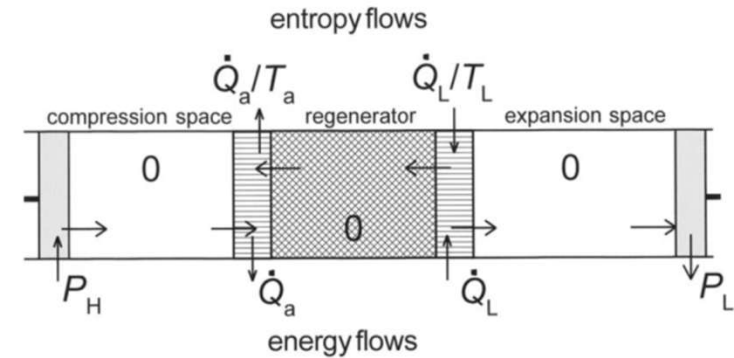
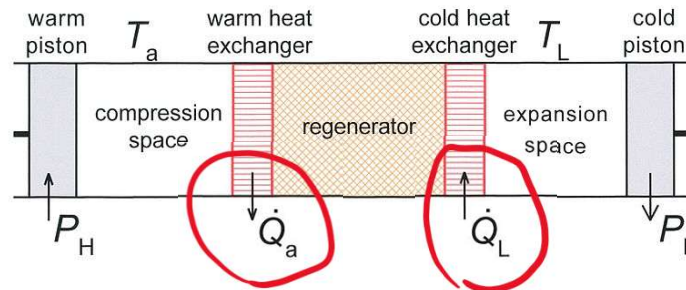
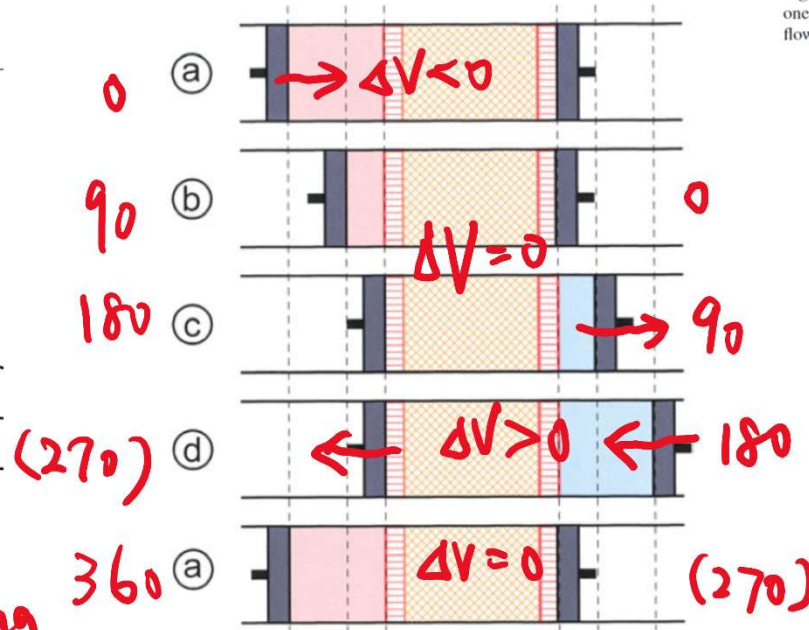
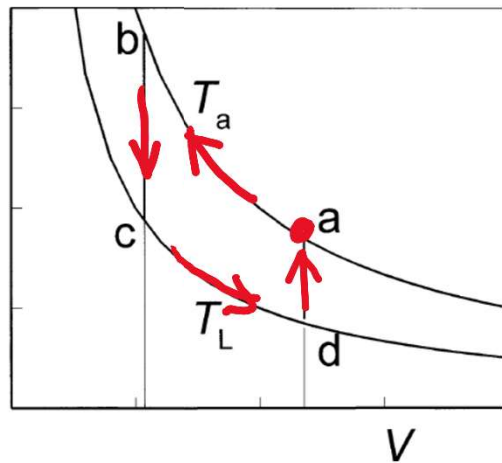


Fig. 9 Schematic diagram of a Stirling cooler. The system has one piston at ambient temperature  $T_a$  and one piston at low temperature  $T_L$ . The upper half shows the entropy flows and the lower half the energy flows

$$\frac{\dot{Q}_a}{T_a} = \frac{\dot{Q}_L}{T_L}.$$

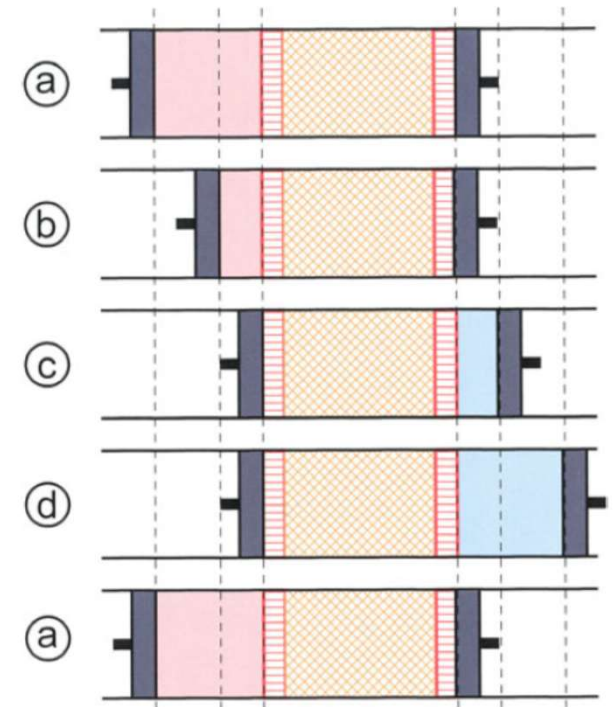
$$\xi = \frac{\dot{Q}_L}{P_H - P_L} = \frac{T_L}{T_a - T_L}.$$



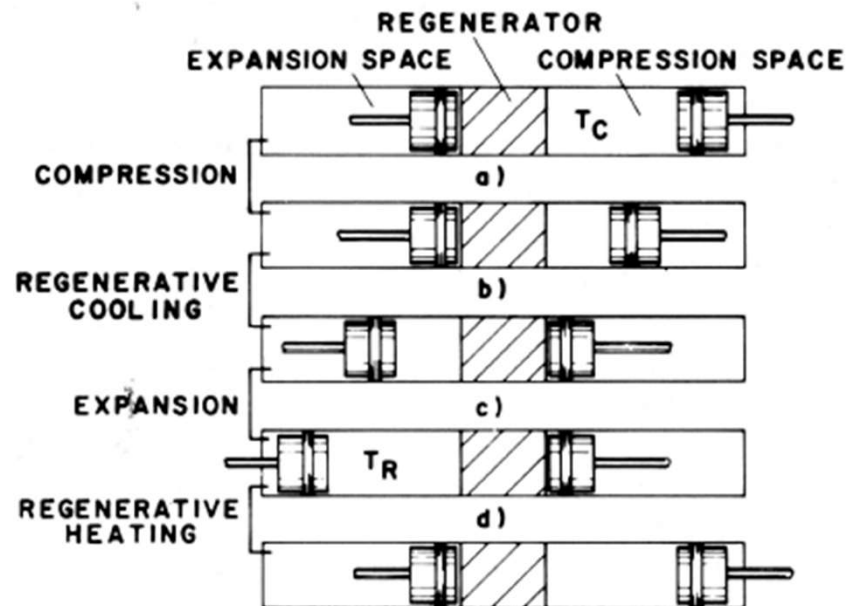
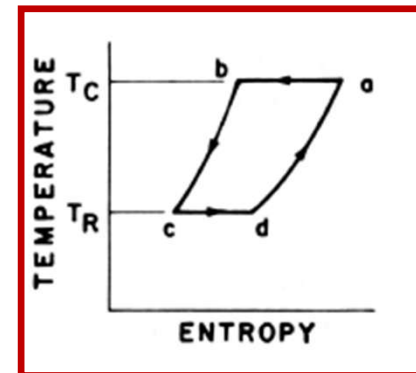
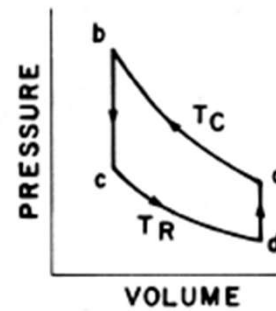
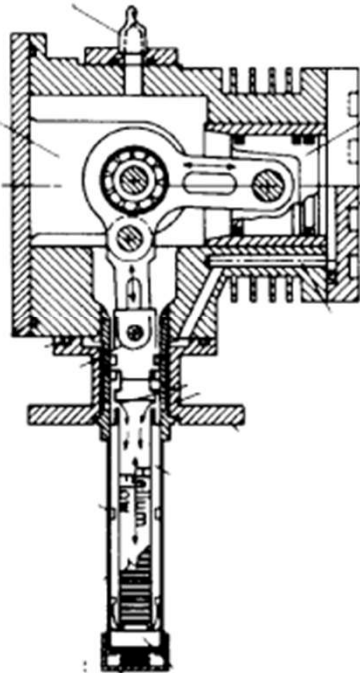
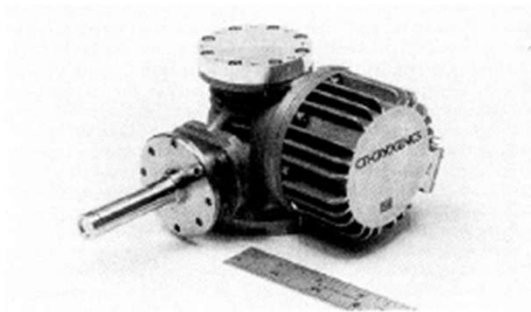
CCW = work → cooling

# Stirling Coolers

1. From a to b. The warm piston moves to the right over a certain distance while the position of the cold piston is fixed. The compression at the hot end is **isothermal** by definition, so a certain amount of heat  $Q_a$  is given off to the surroundings at temperature  $T_a$ .
2. From b to c. Both pistons move to the right so that the **volume between the two pistons remains constant**. The gas enters the regenerator at the left with temperature  $T_a$  and leaves it at the right with temperature  $T_L$ . During this part of the cycle heat is given off by the gas to the regenerator material. During this process the pressure drops and heat has to be supplied to the compression and expansion spaces to keep the temperatures constant.
3. From c to d. The cold piston moves to the right while the position of the warm piston is fixed. The expansion is isothermal so heat  $Q_L$  is taken up from the application.
4. From d to a. Both pistons move to the left so that the total volume remains constant. The gas enters the regenerator at the right with temperature  $T_L$  and leaves it at the left with  $T_a$  so heat is taken up from the regenerator material. During this process the pressure increases and heat has to be extracted from the compression and expansion spaces to keep the temperatures constant. In the end of this step the state of the cooler is the same as at the start.

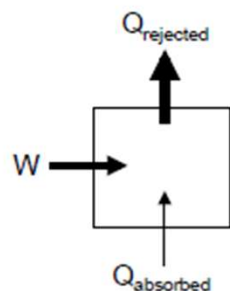


# Stirling Cryocoolers



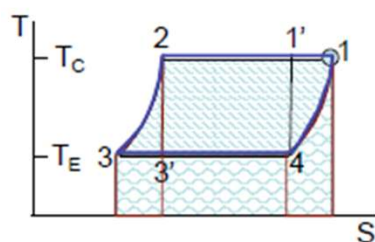


# Stirling Cycle: Zero'th Order (ideal gas) Analysis



- Compare work and heat transfer for Stirling and Carnot cycles
- Use helium gas as quantitative example:  
 $T_C = 300 \text{ K}$ ,  $T_E = 100 \text{ K}$ ,  $P_1 = 1 \text{ atm.}$ ,  $P_2 = 20 \text{ atm.}$
- Note that for an ideal gas in isothermal compression we have:

$$s_2 - s_1 = -R \ln \left( \frac{P_2}{P_1} \right)$$



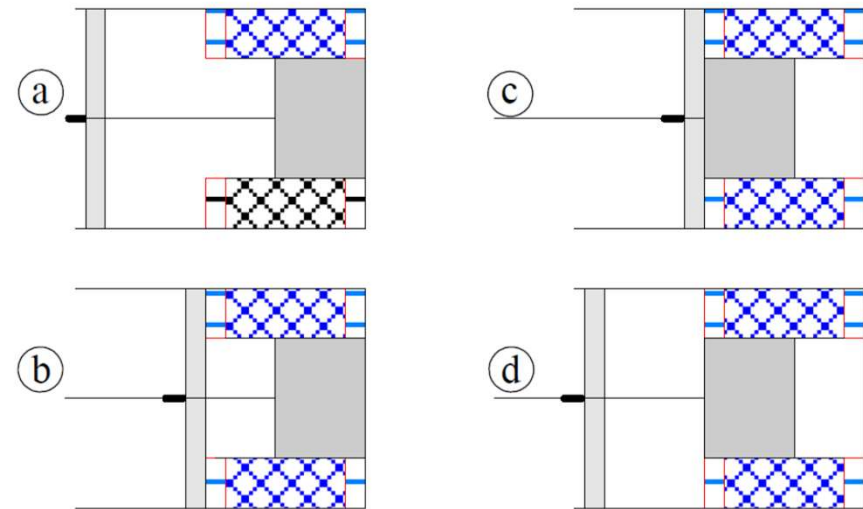
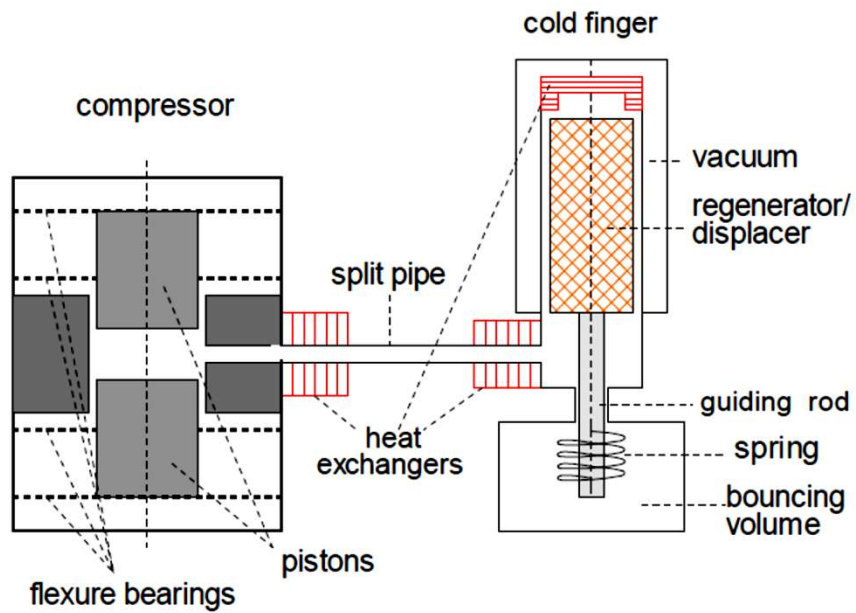
For an ideal cycle

$$\begin{aligned} W_{net} &= Q_r - Q_a \\ &= \oint \delta Q \\ &= \oint T ds \end{aligned}$$

	Carnot		Stirling	
process	$\Delta Q$	helium (J/mol)	$\Delta Q$	helium (J/mol)
● 1(1') - 2	$T_C(s_2 - s_{1'})$	-627	$T_C R \ln(P_1/P_2)$	-4732
● 2 - 3(3')	0	0	$C_v(T_E - T_C)$	-2500
● 3(3') - 4	$T_E(s_4 - s_{3'})$	209	$T_E R \ln(P_3/P_4)$	1577
● 4 - 1(1')	0	0	$C_v(T_C - T_E)$	2500
Net	$(T_C - T_E)(s_2 - s_1)$	-418	$(T_C - T_E) \times R \ln(P_1/P_2)$	-4981
COP	$T_E/(T_C - T_E)$	0.5	$T_E/(T_C - T_E)$	0.5

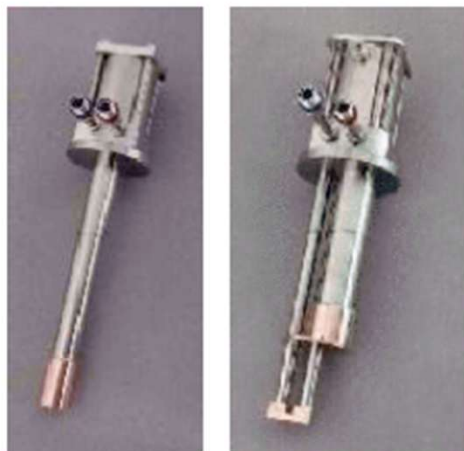
Stirling cycle processes more heat than Carnot cycle, but same efficiency

## free-piston Stirling cooler



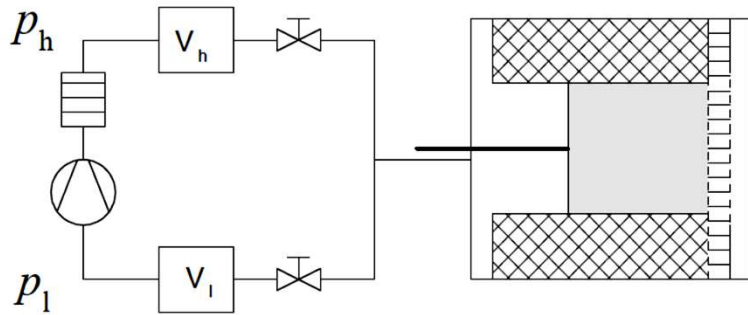
Modified Stirling cycle. The cold piston is replaced by a displacer.

# Gifford-McMahon Cryocooler



- Alternative to Stirling cryocoolers
  - Valving allows use of inexpensive compressors, and separation between cold head and compressor
  - Typical frequency 1 – 2 Hz
  - Somewhat reduced efficiency
  - Cooling power range:
    - ~ 1 watt @ 4.2 K : recondenser
    - 200 watts @ 80 K: cryo-pumps
- Primary uses:
  - Liquid nitrogen plants
  - Cryopumps
  - Conduction cooled s/c magnets - MRI,  $\mu$ SMES, HTS
  - Large scale HTS applications

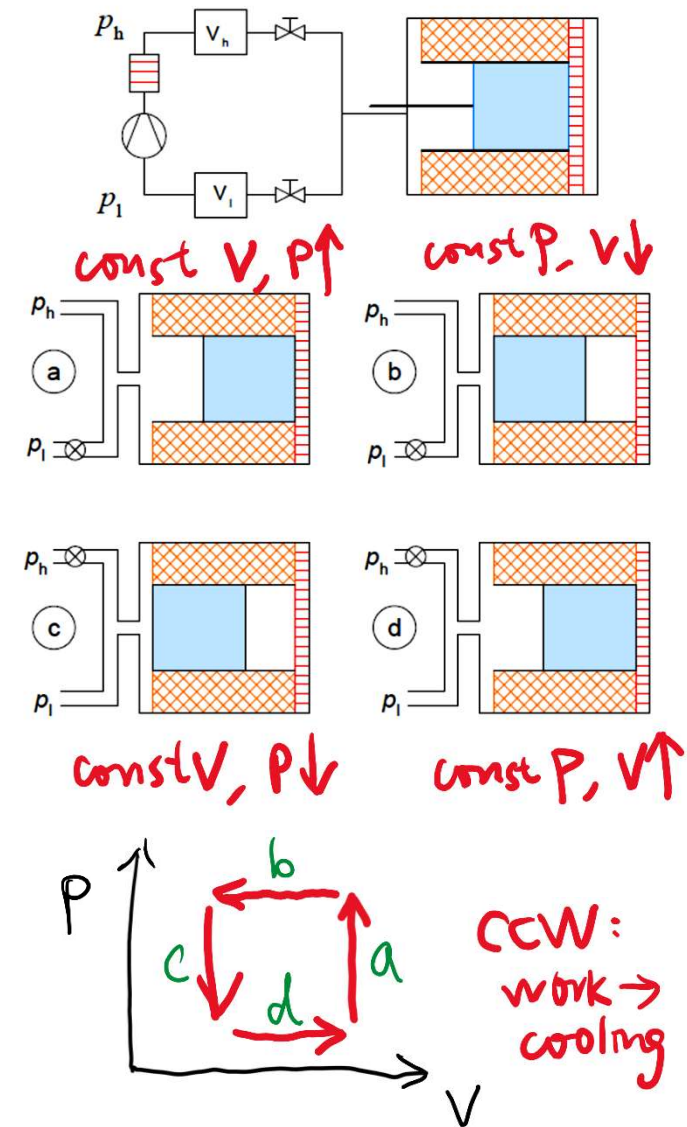
# Gifford-McMahon (GM)-coolers



$V_l$  and  $V_h$  are buffer volumes of the compressor.

The two valves alternatingly connect the cooler to the high- and the low-pressure side of the compressor.

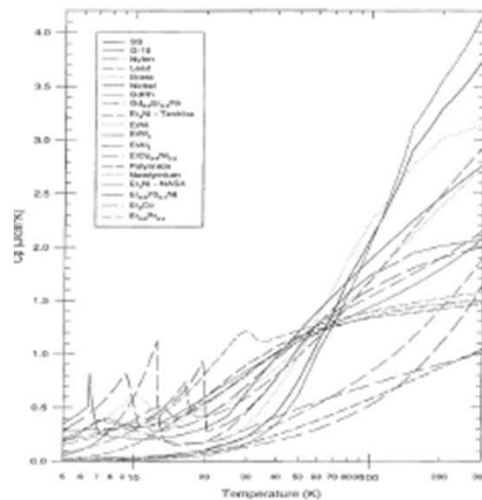
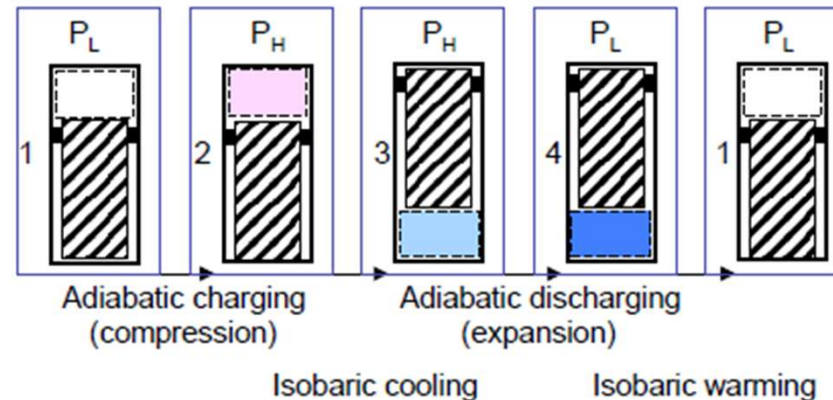
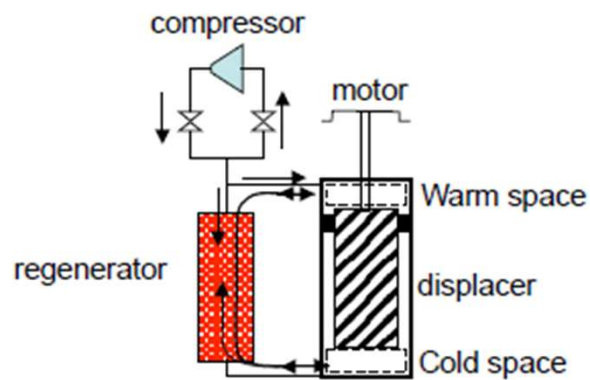
Usually the two valves are replaced by a rotating valve.



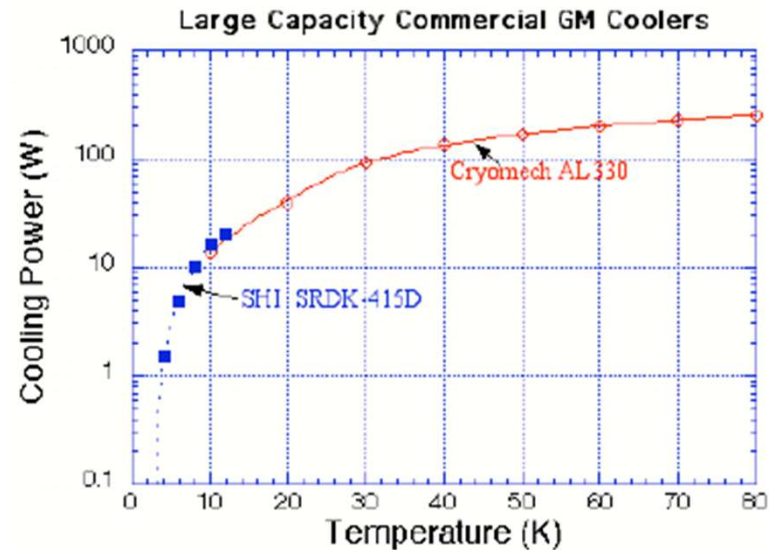


# Gifford-McMahon Cryocoolers

- Cycle description:

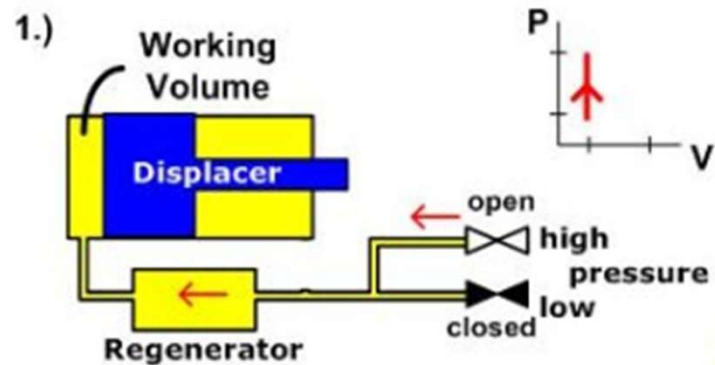


Materials research in the 80's and 90's has enabled 4 K GM machines with cooling capacity ~ 1 watt

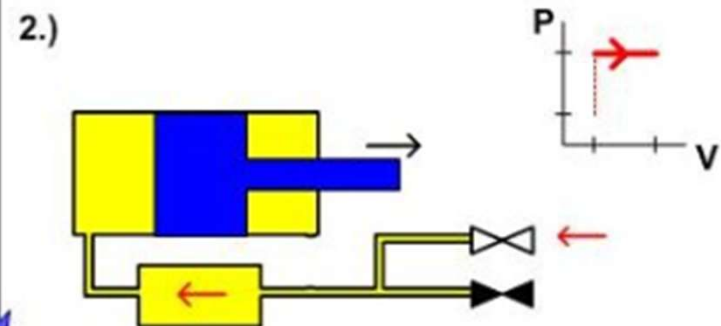




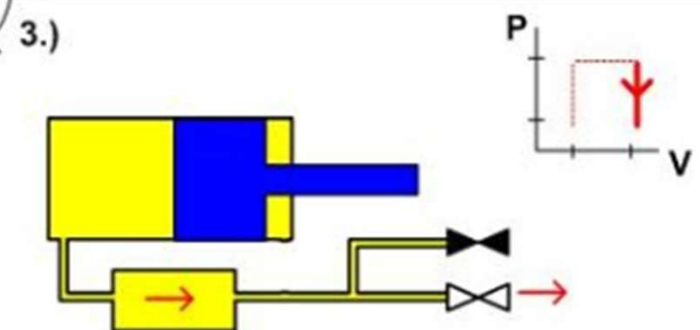
Step 1: pressurize expansion cylinder at minimum volume with regenerated (pre-cooled) gas



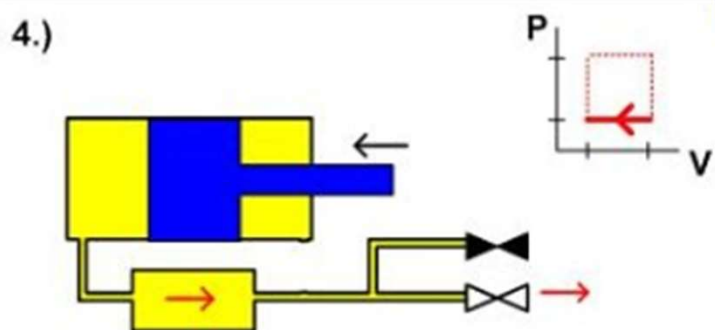
Step 2: maximize volume at max. pressure (more pre-cooled gas added)



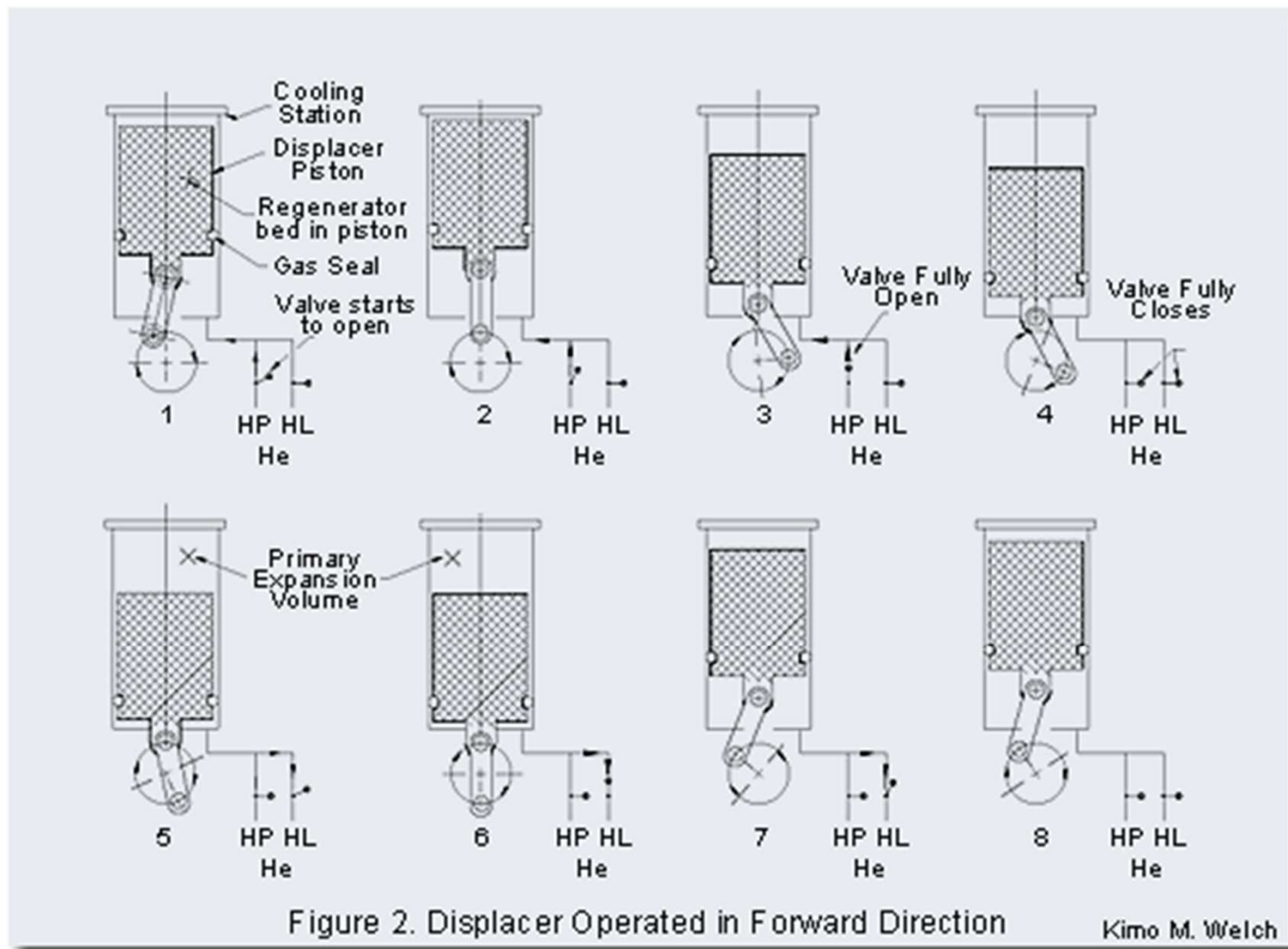
Step 3: de-pressurize and exhaust through the regenerator (cooling)



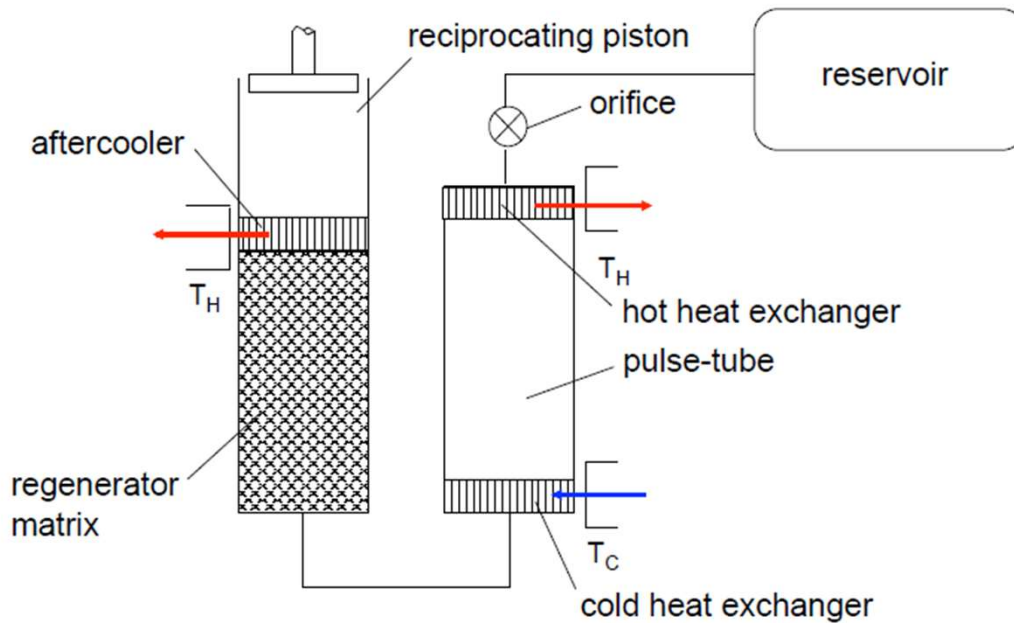
Step 4: minimize volume at min. pressure (more exhaust and regenerator cooling)



Usually the two valves are replaced by a **rotating valve**:

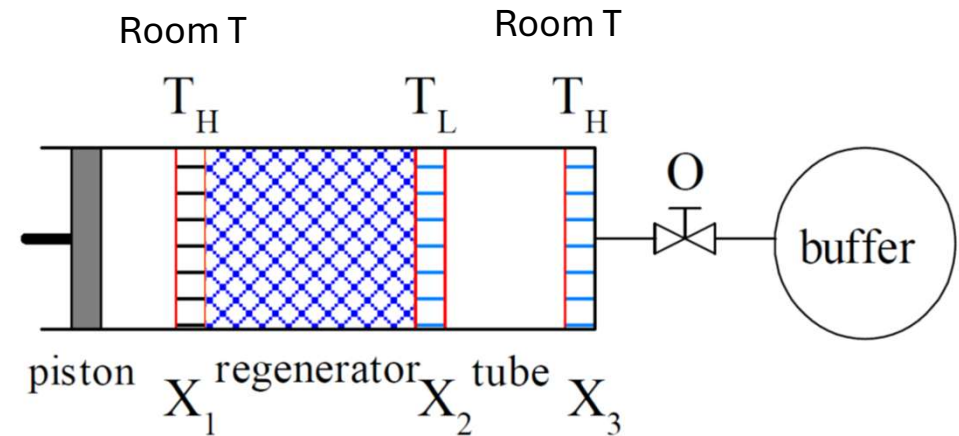


# Stirling type single-orifice Pulse-Tube Refrigerator (PTR)



## Usages:

- Directly liquefy helium gas and recondense boil-off in liquid cryostat
- Direct conductive cooling in dry cryostats (including low vibration options)



From left to right the system consists of a

- A compressor with moving piston (piston),
- the after cooler (X<sub>1</sub>), a regenerator,
- a low-temperature heat exchanger (X<sub>2</sub>),
- a tube (tube),
- a second room-temperature heat exchanger (X<sub>3</sub>),
- an orifice (O), and
- a buffer.

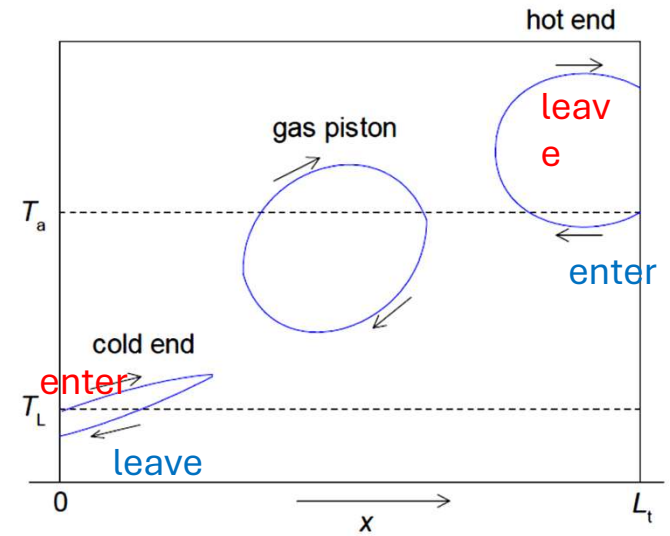
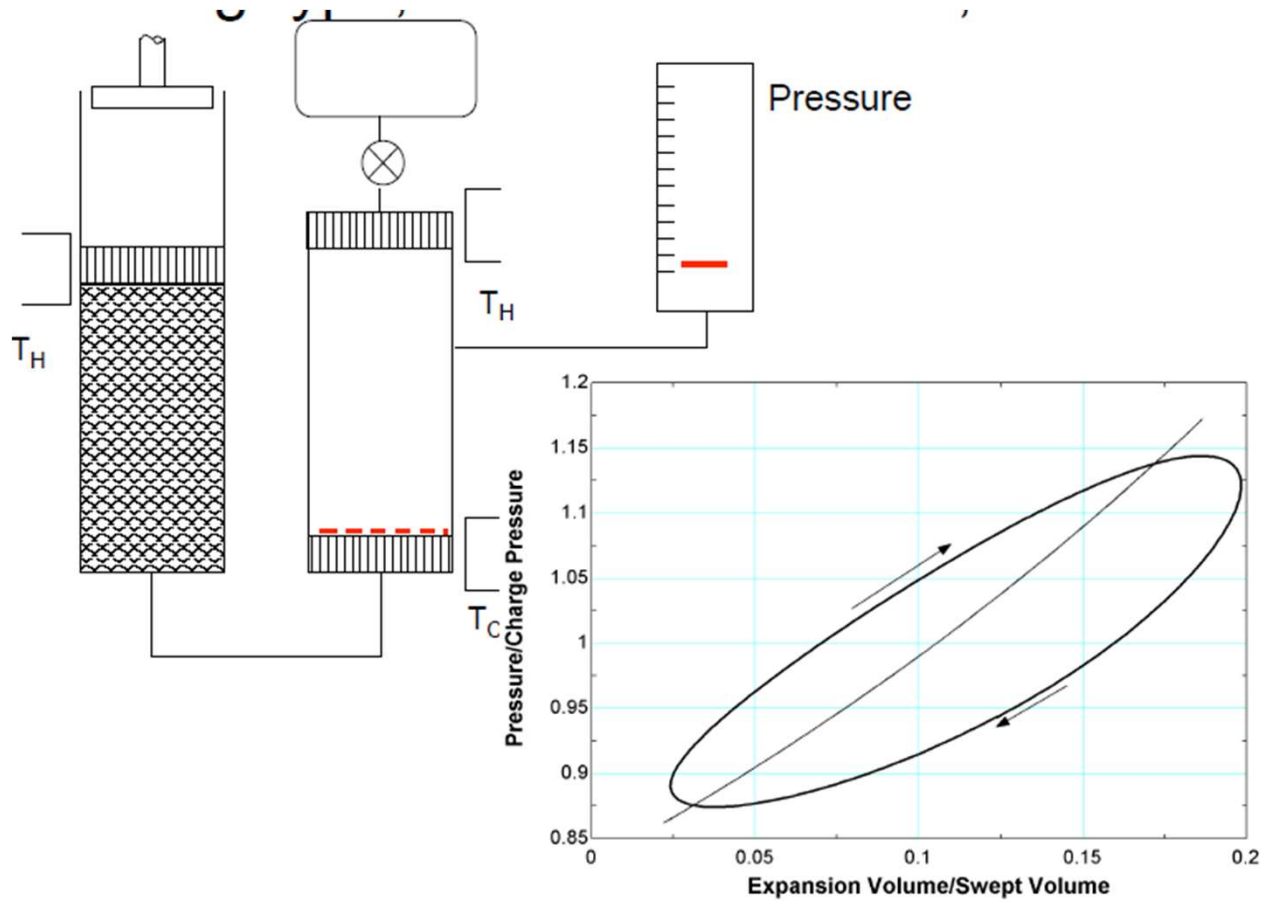
The system is filled with helium at an average pressure of typically 20 bar. .

Room temperature is  $T_H$ .

The cooling power is generated at the low temperature  $T_L$ .

The part in-between the heat exchangers X<sub>1</sub> and X<sub>3</sub> is below room temperature.

# Stirling-type, Orifice Pulse-Tube



# Design Starting Point

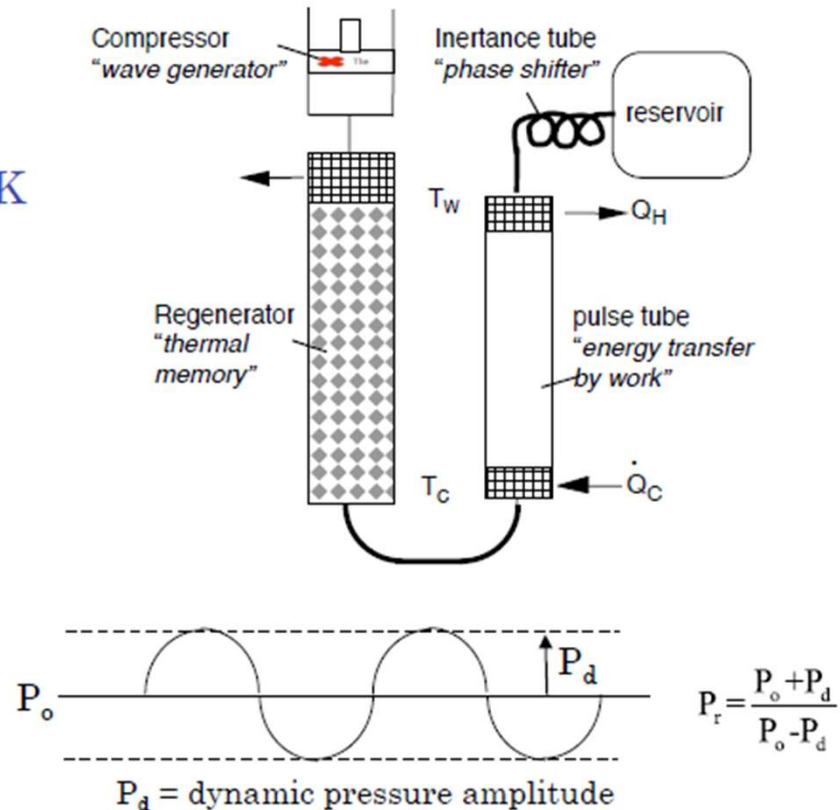
- Desired performance:
  - $\dot{Q}_c @ T_c$  25 watts @ 80 K

- Required definition:

- $T_w$  300 K
- $P_o$  2.5 MPa
- $P_r$  1.3
- $f$  60 Hz

- Design goals:

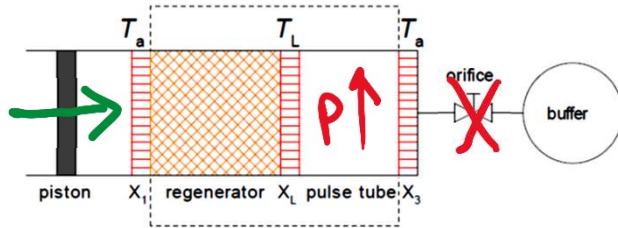
- geometry (L, D) for each component
- Acoustic power
- $\theta$  : phase angle between mass flow & pressure oscillations



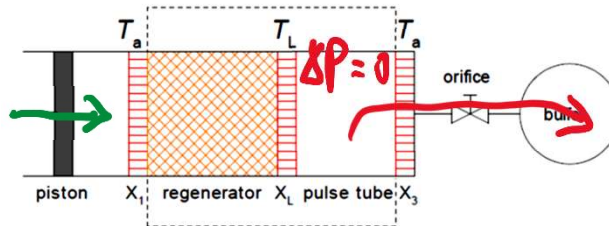


# An idealized cycle

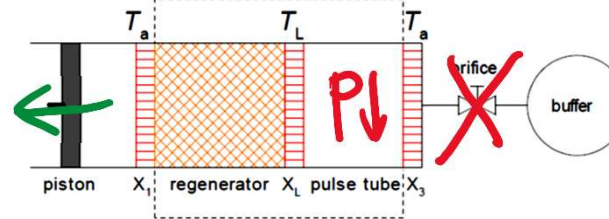
The piston moves the gas back and forth and generates a varying pressure in the system.



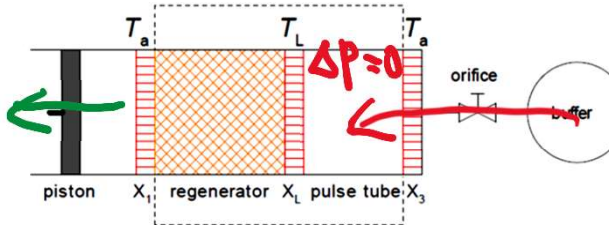
**1. from a via b to c.** The piston moves to the right with the orifice is closed. The pressure rises.



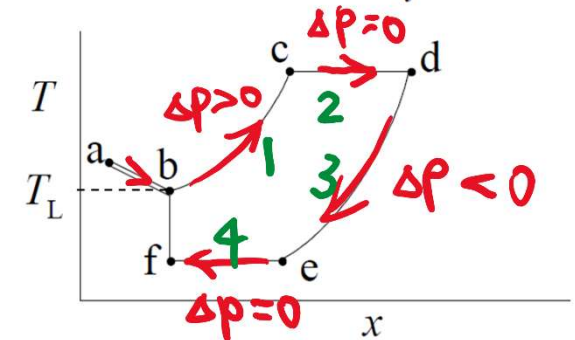
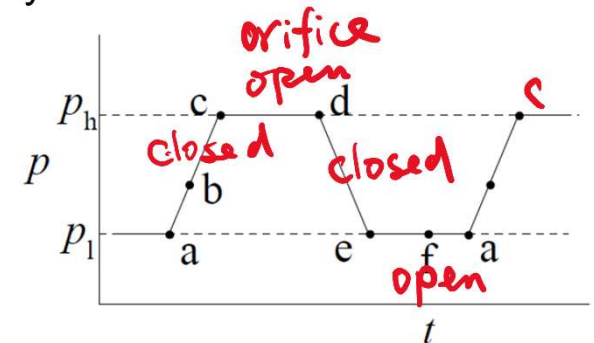
**2. c to d.** The orifice is opened so that gas flows from the tube to the buffer. At the same time the piston moves to the right in such a way that the pressure in the tube remains constant.



**3. d to e.** The piston moves to the left with the orifice is closed. The pressure drops.



**4. e via f to a.** The orifice is opened so that gas flows from the buffer into the tube. At the same time the piston moves to the left so that the pressure in the tube remains constant.



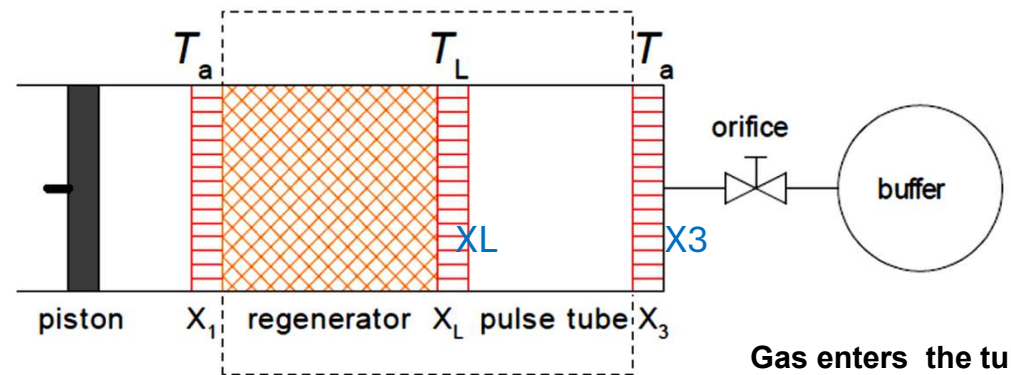
$x$ : fraction of gas in the pulse tube

The piston moves the gas back and forth and generates a varying pressure in the system. The pressure varies smoothly at  $f=1\text{-}50\text{Hz}$

- There are no acoustic effects, such as travelling pressure waves, or fast pressure changes (pulses).
- In the regenerator and in heat exchangers, the gas is in good thermal contact with its surroundings *while in the tube the gas is thermally isolated*.

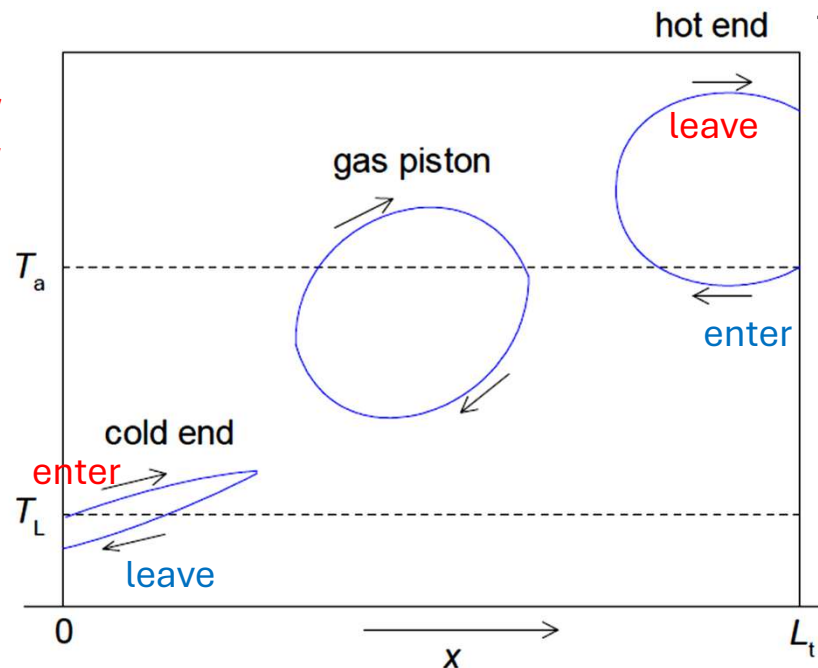
**Gas elements inside the tube are compressed or expanded adiabatically and reversibly, so their entropy is constant. Compression leads to heating and expansion to cooling.**

At the **cold end** of the tube, the gas leaves the cold heat exchanger  $X_L$ , and enters the tube when the pressure is high and temperature  $T_L$ . **It returns to  $X_L$ , when the pressure is low** and the temperature is below  $T_L$ . Hence producing cooling.



Gas enters the tube if  $p_t < p_B$  and leaves the tube if  $p_t > p_B$ . So the final pressure is larger than the initial pressure.

Gas enters the tube at temperature  $T_H$  and leaves it at a higher temperature producing **heating**. Heat is released via the heat exchanger  $X3$  to the surroundings and the gas flows to the orifice at ambient temperature.



Temperature-position curves of two gas elements (one at the cold end and one at the hot end)

# Thermodynamics of PTR's

(a) At the **hot end**, gas flows from the buffer via the orifice into the tube with a temperature  $T_H$  if the pressure  $p_t$  is below the pressure in the buffer  $p_B$  ( $p_t < p_B$ ).

If  $p_t = p_B$  the gas at the hot end comes to a halt.

If  $p_t > p_B$  the gas moves to the hot end of the tube and through the heat exchanger X and the orifice into the buffer.

**So gas elements enters the tube if  $p_t < p_B$  and leaves the tube if  $p_t > p_B$ .**

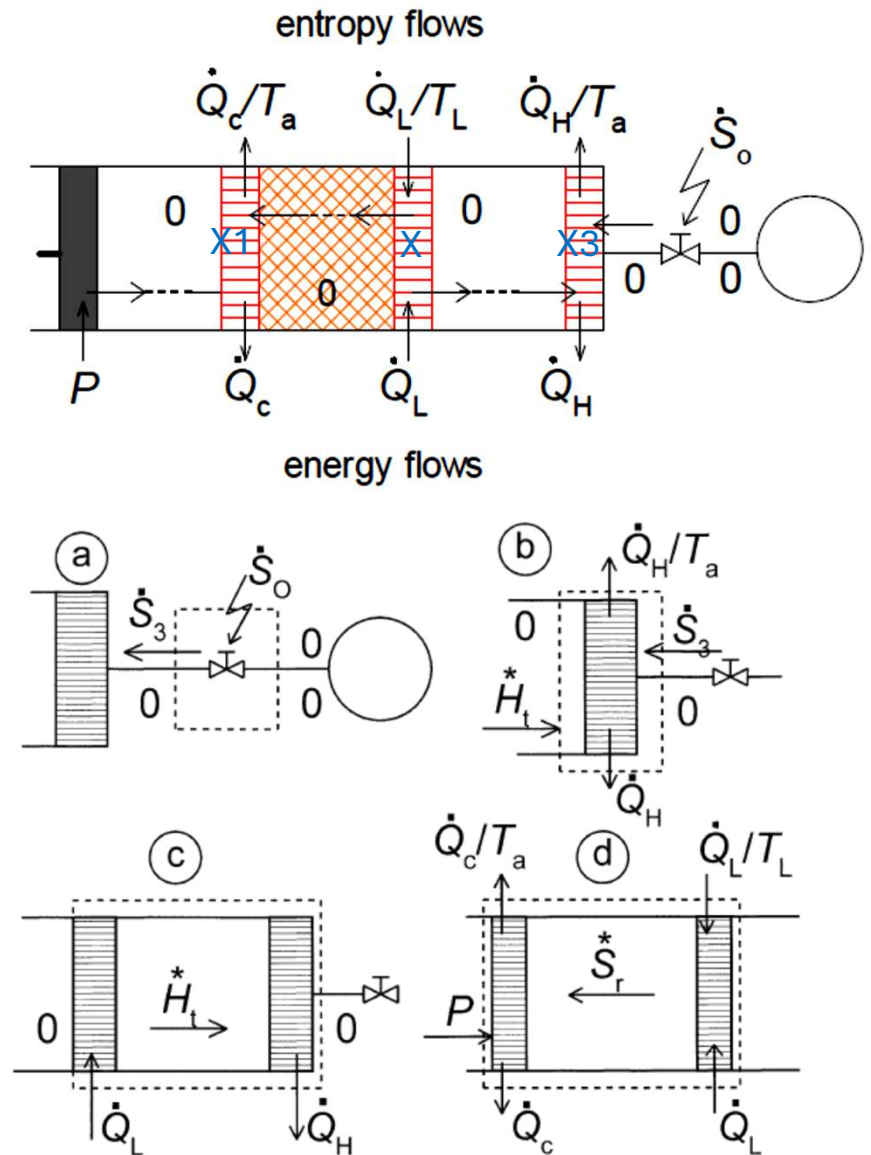
So the final pressure is larger than the initial pressure.

Consequently, the gas leaves the tube with a temperature higher than the initial temperature  $T_H$ .

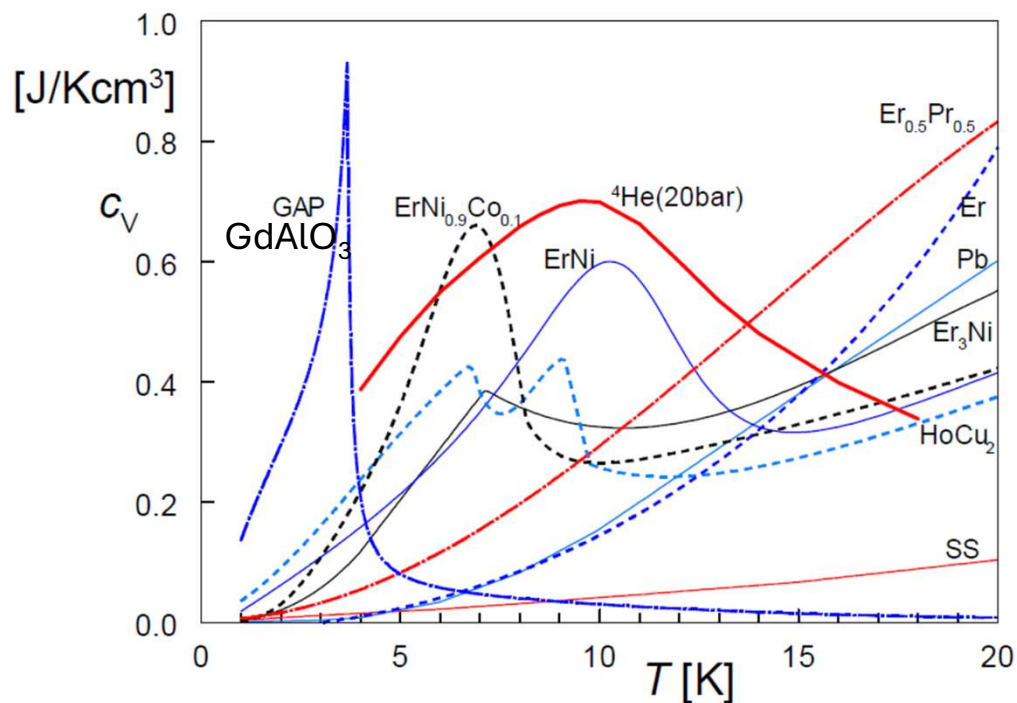
(b) Heat is released via the heat exchanger X3 to the surroundings and the gas flows to the orifice at ambient temperature.

(c) At the **cold end** of the tube, the gas leaves the cold heat exchanger X, and enters the tube when the pressure is high and temperature  $T_L$ . It returns to X, when the pressure is low and the temperature is below  $T_L$ . Hence producing cooling.

The analysis of the situation at the cold end is a bit more complicated due to the fact that the velocity at the cold end is determined by the velocity of the gas at the hot end and by the elasticity of the gas column in the tube. Still the situation is basically the same.



# Regenerator: materials



The thermodynamic and hydrodynamic properties of regenerators usually are extremely complicated. In many cases it is necessary to make simplifying assumptions. In its most extreme form in an ideal regenerator:

1. the **heat capacity of the matrix** is much larger than of the gas;
2. perfect heat contact between the gas and the matrix
3. the gas in the regenerator is an ideal gas;
4. Zero flow resistance of the matrix;
5. Zero axial thermal conductivity;
6. Zero void volume of the matrix is zero.

If conditions 1 and 2 are satisfied, then the gas **temperature at a certain point in the regenerator is constant**.

If, in addition, condition 3 is satisfied as well, then the **average enthalpy flow in the regenerator is zero**.

If conditions 2, 4, and 5 are satisfied, there are no irreversible processes in the regenerator.

**Ideal PTR: dissipation only occurs in the orifice**



# PTR

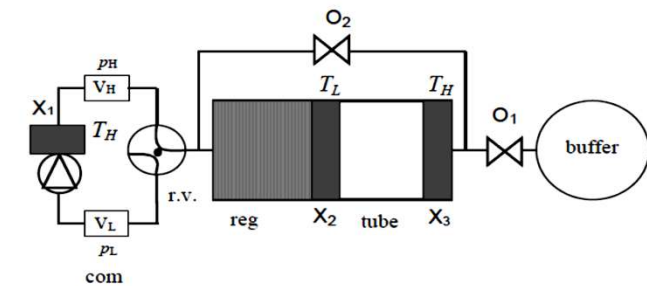
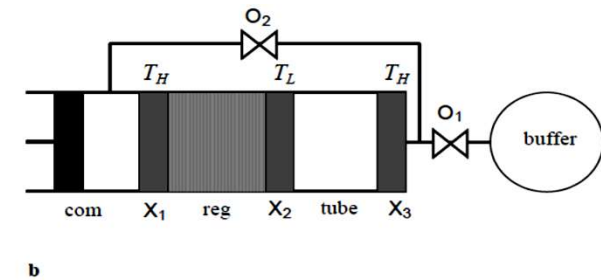
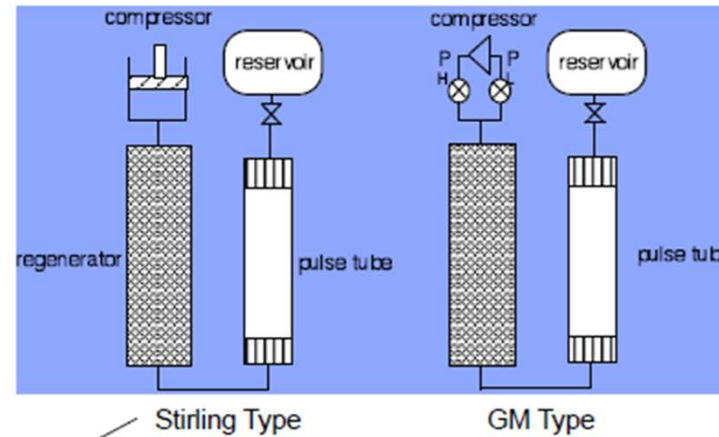
## Two general types

### – Stirling type

- High frequency  $\sim 60$  Hz
- High efficiency: 25% of Carnot
- Operation down to 10 K

### – GM type

- Low frequency  $\sim 1$ -2 Hz
- Split design = very low vibration
- Ideal for 4 K operation ( $\leq 1$  watt)



1. Two types of the PTR. (a) A Stirling-type PTR. From left to right it consists of a compressor aftercooler ( $X_1$ ), a regenerator (reg), a cold heat exchanger ( $X_2$ ), a pulse tube (tube), a hot heat ( $X_3$ ), an orifice ( $O_1$ ), and a buffer. Orifice  $O_2$  connects the hot end of the regenerator and the hot pulse tube. (b) A GM-type PTR. Except for the compressor - rotary valve (r.v.) combination, the ponents of the GM-type PTR are the same as of the Stirling PTR.



MD 200

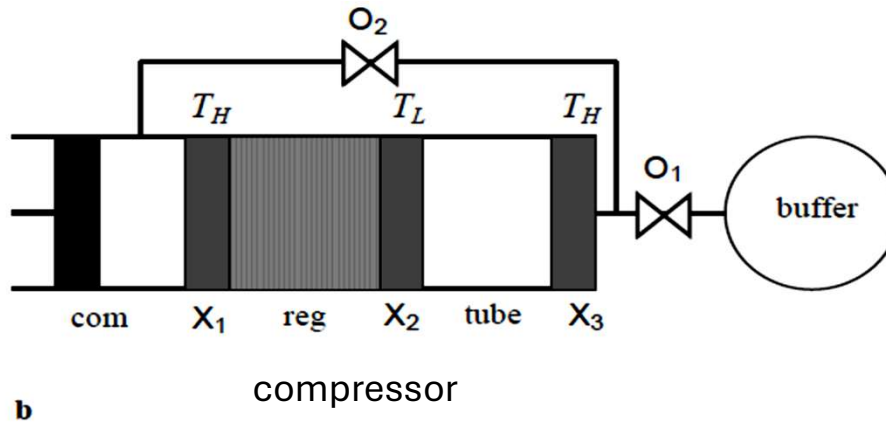


Cryomech PT405

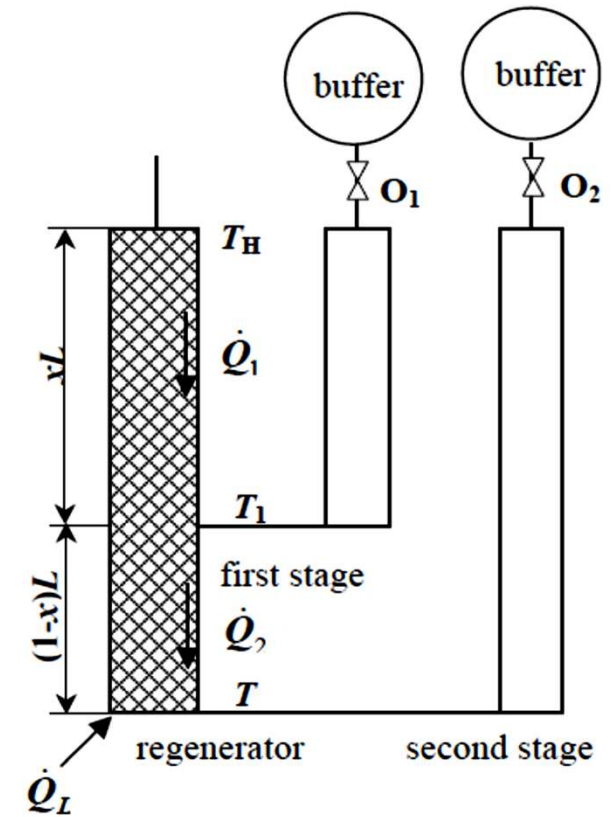
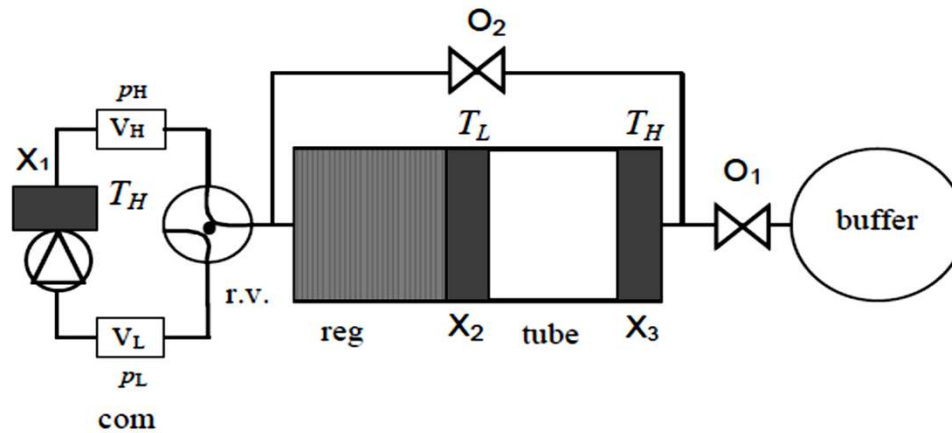




## Stirling-type PTR

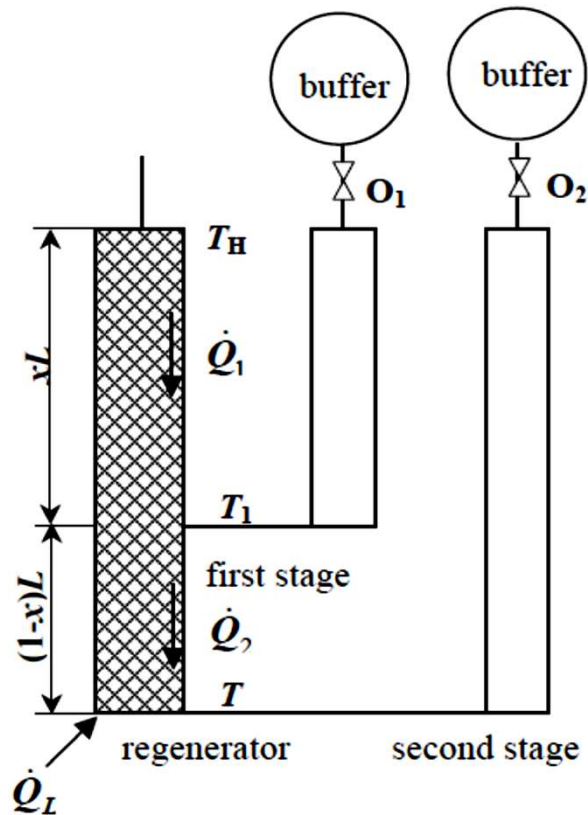


## GM-type PTR



Two-stage single-orifice PTR. It has a cooling power  $\dot{Q}_L$  at  $T_2$ . The heat flow  $\dot{Q}_1$  and  $\dot{Q}_2$  are caused by heat conduction.

**Figure 2. 1.** Two types of the PTR. (a) A Stirling-type PTR. From left to right it consists of a compressor (com), an aftercooler ( $X_1$ ), a regenerator (reg), a cold heat exchanger ( $X_2$ ), a pulse tube (tube), a hot heat exchanger ( $X_3$ ), an orifice ( $O_1$ ), and a buffer. Orifice  $O_2$  connects the hot end of the regenerator and the hot end of the pulse tube. (b) A GM-type PTR. Except for the compressor - rotary valve (r.v.) combination, the main components of the GM-type PTR are the same as of the Stirling PTR.



- The PTR has no moving parts in the low-temperature region, and, therefore, has a **long lifetime and low mechanical and magnetic interferences**. →
  - Long mean time between maintenance
  - Minimal general maintenance
  - Ideal for vibration sensitive applications
- A typical average pressure in a PTR is 10 to 25 bar, and a typical pressure amplitude is 2 to 7 bar.
- A piston compressor (in case of a *Stirling type PTR*) or a combination of a compressor and a set of switching valves (*GM type PTR*) are used to create pressure oscillations in a PTR.

## Standard 4K Cryomech Single-Stage Pulse Tube Cryorefrigerators

All models have remote-motor options available, Air or Water Cooled



**PT 10**  
•12W @ 80K



**PT 60**  
•60W @ 80K

**PT 63**  
•23W @ 40K



**PT 90**  
•90W @ 80K



**PT 403**  
First Stage 7W @ 65K  
Second Stage 0.25W @ 4.2K



**PT 405**  
First Stage 25W @ 65K  
Second Stage 0.5W @ 4.2K

**PT 407**  
First Stage 25W @ 55K  
Second Stage 0.7W @ 4.2K



**PT 415**  
First Stage 40W @ 45K  
Second Stage 1.5W @ 4.2K

# CRYOMECH

## Cryorefrigerator Specification Sheet

### PT405 with CP2850

#### Cold head

Cooling capacity @ 50 and 60 Hz:  
2<sup>nd</sup> stage and 1<sup>st</sup> stage combined

Lowest temperature  
Cool down time

Weight  
Dimensions

PT405

0.5W @ 4.2K with 25W @ 65K

2.8K with no load  
60 minutes to 4K

32 lb (14.5 kg)  
See cold head line drawing

#### Compressor package

Water cooled:

Weight  
Dimensions - L x W x H

Electrical rating  
Power consumption @ steady state  
Cooling water flow rate

CP2850, available as water or cooled

243 lb (110 kg)

19 x 18 x 24.5 in (48 x 46 x 62 cm)

200/230 or 440/480VAC, 3Ph, 60Hz // 200 or 380/415VAC, 3Ph, 50Hz

4.9 kW // 5.4 kW

Minimum flow 2.3 GPM (9 LPM) @ 80°F (27°C) maximum temperature

Air cooled:

Weight  
Dimensions - L x W x H

Electrical rating  
Power consumption @ steady state

384 lb (174 kg)

23.5 x 21 x 43 in (60 x 54 x 109 cm)

200/230 or 440/480VAC, 3Ph, 60Hz // 200 or 380/415VAC, 3Ph, 50Hz

5.5 kW // 6.0 kW

#### Flexible lines

Standard length  
Weight per pair

10 ft (3 m)

9.2 lb (4.2 kg)

#### System parameters

Helium pressure

Ambient temperature range

220 ± 5 PSIG (15.2 ± .34 bar) @ 60 Hz

250 ± 5 PSIG (17.2 ± .34 bar) @ 50 Hz

45°F to 100°F (7 to 38°C)

#### Maximum sound level

Water cooled

Air cooled

70 dBA @ 1 meter

74 dBA @ 1 meter

#### Shipping crate

Water cooled:

Weight  
Dimensions - L x W x H

Wood box

455 lb (206 kg)

48 x 40 x 38 in (122 x 102 x 97 cm)

Air cooled:

Weight  
Dimensions - L x W x H

635 lb (288 kg)

48 x 40 x 59 in (122 x 102 x 150 cm)

113 Falso Drive, Syracuse, NY 13211 USA  
315.455.2555 v 315.455.2544 f cryosales@cryomech.com www.cryomech.com

Specifications subject to change without notice.

Revised 29AUG13

# PT 405

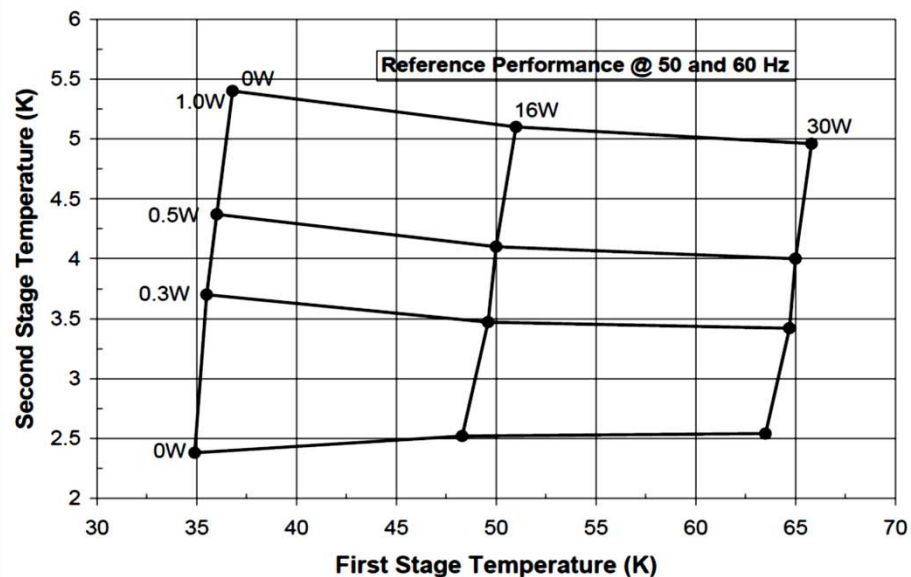
## PT 405

First Stage 25W @ 65K

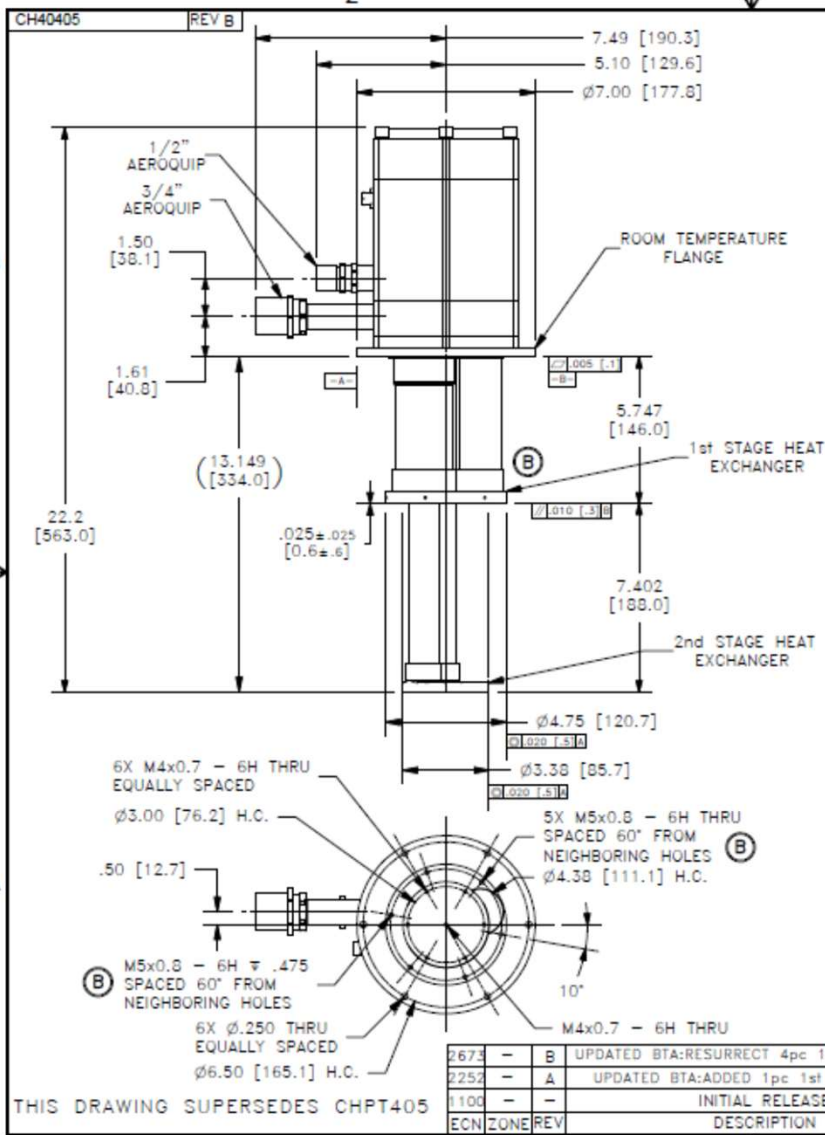
Second Stage 0.5W @ 4.2K

# CRYOMECH

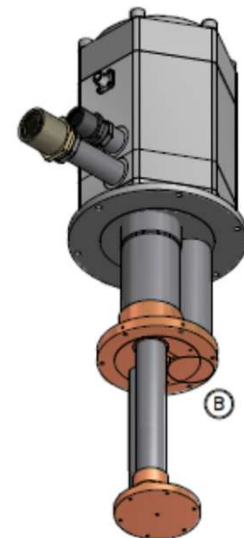
## PT405 Cryorefrigerator Capacity Curve



Certified Performance: 0W < 2.8K  
0.5W@4.2K with 25W@65K



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**\*\*SPECIAL NOTE: COLDHEAD MUST BE OPERATED COLD END DOWN\*\***

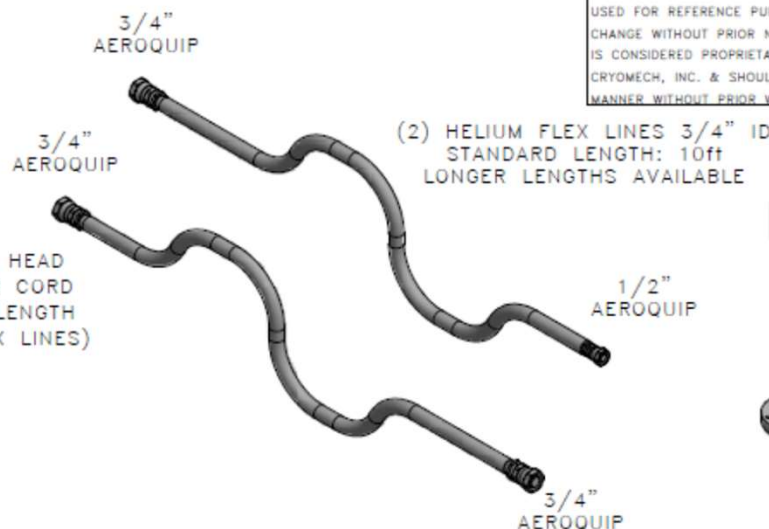
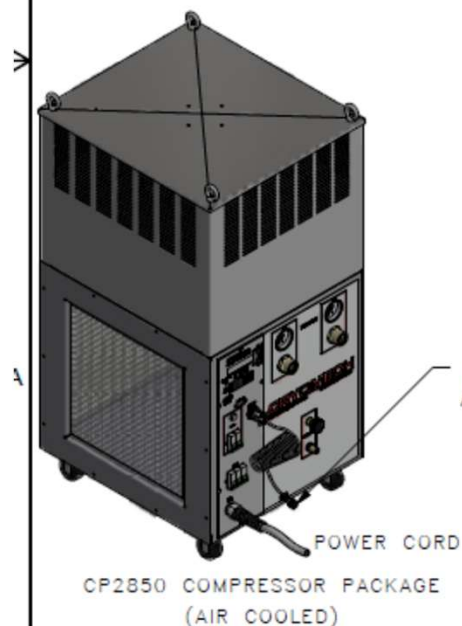
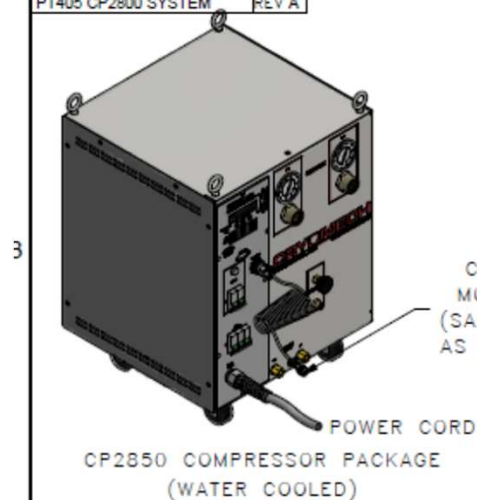
THIRD ANGLE PROJECTION		CRYOMECH, INC.	
		113 FALSO DRIVE SYRACUSE, N.Y. 13211	
		Tel: (315)455-2555 Fax: (315)455-2544	
ALL DIMENSIONS ARE IN INCHES			
TOLERANCES: FRACTIONS ±1/32 DECIMALS XXX±.005 XX ±.01 X±.1			
ANGLES ±5° ALLOWER FINISH 25 Ra			
CONCENTRICITY .005 TOTAL INDICATOR RUN OUT			
PERPENDICULAR ±.002 (UNLESS OTHERWISE SPECIFIED)			
NAME: CH40405 COLDHEAD OUTLINE			
DWG #: CH40405		SHT 1 OF 1	
MATERIAL: 103-18			
2675	-	B	UPDATED BTA:RESURRECT 4pc 1st STAGE HT EX
2252	-	A	UPDATED BTA:ADDED 1pc 1st STAGE HT EX
1100	-	-	INITIAL RELEASE
ECN	ZONE	REV	DESCRIPTION
19AUG11			
05OCT10			
25MAY06			
DATE			
OWN BY: KDJ	DATE: 09JAN03	SCALE: .175	DWG SIZE: A
1ST CHK: KAH	DATE: 09JAN03	2ND CHK: RED	DATE: 09JAN03
CUST: -		BTA: BTA-PT405/PT407	





PT405 CP2800 SYSTEM REV A

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PT405 COLD HEAD

MANUAL

TOOL KIT



**CRYOMECH, INC.**  
113 FALSO DRIVE SYRACUSE, N.Y. 13211  
Tel: (315)455-2555 Fax: (315)455-2544

ALL DIMENSIONS ARE IN INCHES  
TOLERANCES: FRACTIONS  $\pm 1/32$  DECIMALS  $\pm .005$  XX  $\pm .01$  X  $\pm .1$   
ANGLES  $\pm .5^\circ$  ALLOVER FINISH 25 Ra  
CONCENTRICITY .005 TOTAL INDICATOR RUN OUT  
PERPENDICULAR  $\pm .002$  (UNLESS OTHERWISE SPECIFIED)

NAME: PT405 CP2800 CRYOREFRIGERATOR

DWG #: PT405 CP2800 SYSTEM

SHT 1 OF 1

MATERIAL: AS STATED

5072	-	A	ADDED AIR COOLED COMPRESSOR	21MAY13
1436	-	-	INITIAL RELEASE	14AUG07
ECN	ZONE	REV	DESCRIPTION	DATE

DWN BY: BMR	DATE: 14AUG07	SCALE: TO FIT	DWG SIZE: A
1ST CHK: RED	DATE: 21AUG07	2ND CHK: AO	DATE: 21AUG07
CUST:		BTA:	

# Sumitomo pulse-tubes



## Specifications

Cold Head Model		<a href="#">RP-062B</a>	<a href="#">RP-062BS</a>	<a href="#">RP-082B2</a>	<a href="#">RP-082B2S</a>
1 <sup>st</sup> Stage Capacity	50 Hz	30 W @ 65 K	25 W @ 65 K	45 W @ 45 K	35 W @ 45 K
	60 Hz	30 W @ 65 K	25 W @ 65 K	45 W @ 45 K	35 W @ 45 K
2 <sup>nd</sup> Stage Capacity	50 Hz	0.5 W @ 4.2 K	0.4 W @ 4.2 K	1.0 W @ 4.2 K	0.9 W @ 4.2 K
	60 Hz	0.5 W @ 4.2 K	0.4 W @ 4.2 K	1.0 W @ 4.2 K	0.9 W @ 4.2 K
Minimum Temperature <sup>1</sup>		<3.0 K	<3.0 K	<3.0 K	<3.0 K
Cooldown Time	50 Hz	<100	<100	<80	<90
	60 Hz	<90	<90	<80	<90
Weight		23.2 kg (51.2 lbs.)	23.5 kg (51.8 lbs.)	26.0 kg (57.3 lbs.)	26.0 kg (57.3 lbs.)

## Helium Reliquefiers

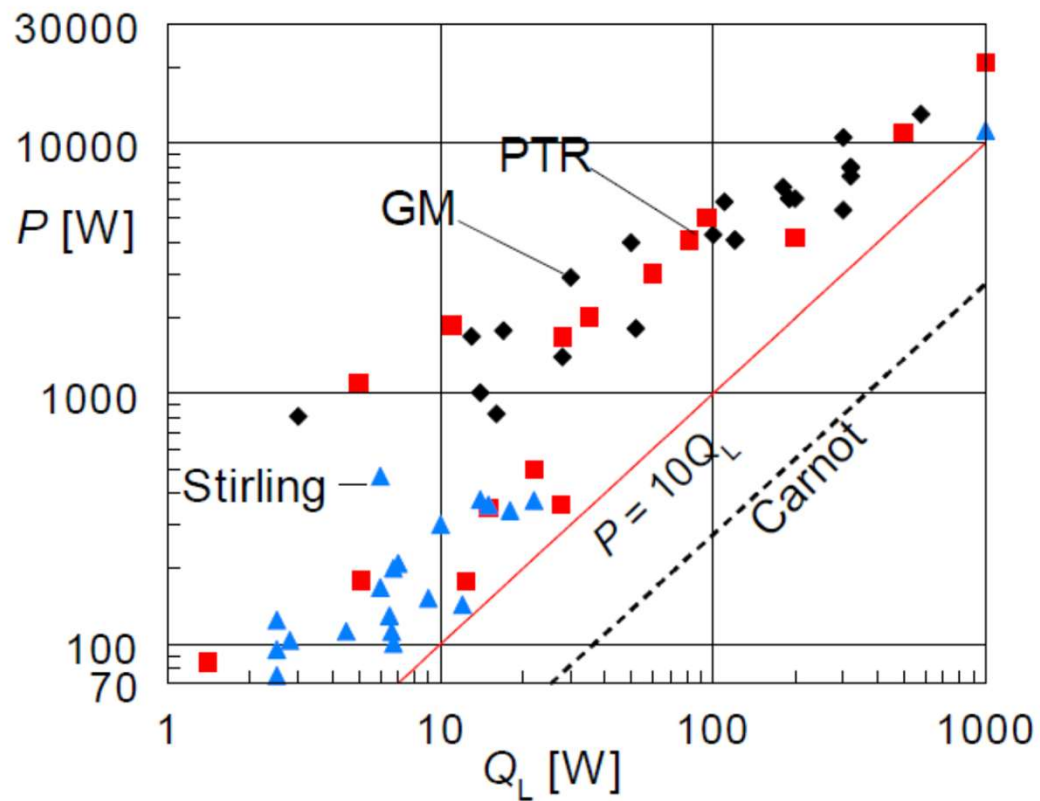


## Pulse Tubes: Future Directions & Commercial Sources

- R&D:
  - Phase shifting mechanisms - inertance tubes
  - Large capacity - modeling & losses
  - Performance improvements
- Sources:
  - GM-type
    - Cryomech, SHI (Sumitomo Heavy Industry), U of Giessen,
  - Stirling type
    - Atlas Scientific, STC, Sunpower, TRW, Martin-Marietta, Praxair, Sierra-Lobo



values at 80 K



**Homework (before next Tuesday):**

watch this youtube video to learn about superfluid helium:

[John Allen's Movie about Superfluid Helium](#)